

**Solar Heater the principle and the design the extra corrected version—2011/3/1,**

The aim of this topics is survey what type of SH is best performance from view of physics principle and of costs for materials. Many useful concrete topics were found, but the principle for **design calculator** is difficult to find. Hereupon 2011/2/4 the first version was found to have many articles which should be corrected and supplemented. Here are summary for those problems.

—Note for correction and supplement for "red characters"—

**① [ 3 ] : Green House Effect Box without solar ray focusing.**

This chapter has many doubtful points.

\*Conductive and convection heat flow loss ( $\equiv Q_{C\&V}$ ) are almost negligible.

But reality could not be so,

\* $(2) Q_s = Q_L = S_L \sigma T^4$ .  $\rightarrow (3) T_M = [Q_s / S_L \sigma]^{1/4}$ . <equilibrium max temperature>>

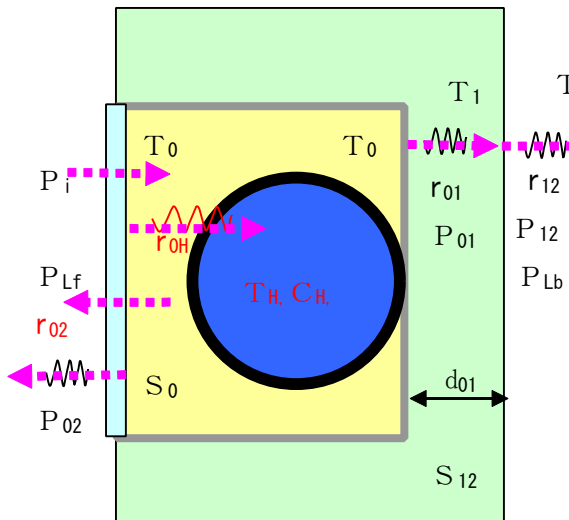
$\rightarrow Q_s = Q_L = Q_{C\&V} + S_L \sigma T^4$ .  $\rightarrow (3) T_M = [(Q_s - Q_{C\&V}) / S_L \sigma]^{1/4} = [(Q_s - Q_{C\&V}) / S_L \sigma]^{1/4}$ .

<<equilibrium max temperature, but is not pragmatism utility one>>

Note that half mirror  $\epsilon = 1$  (blackbody) when top cover would become  $T_M$  ③.

Following is a heat box model of **heat input and outputs account**.

Heat Box Model.



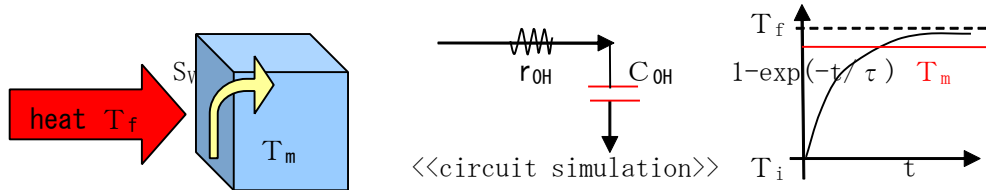
heat resistor definition:  
 $P_{01} = (T_0 - T_1) \kappa_{01} / d_{01}$ .  
 $\rightarrow r_{01} \equiv (T_0 - T_1) / P_{01} = d_{01} / \kappa_{01}$ .  
 It's quite analogy of electrical circuit of current P and voltage T.

$P_i = S_0 P_0$ . << $P_0 = 956 \text{ W/m}^2$ >>  
 $P_{Lf} = S_0 \epsilon \sigma T_0^4 + S_{12} \epsilon_{12} \sigma T_1^4$ .  
 $-(S_0 + S_{12}) \sigma T_2^4$ .  
 $\equiv$  radiation outgoing-incoming.  
 $P_{Lb} = P_{02} + P_{01} (= P_{12}) = (T_0 - T_2) / r_{02} + (T_0 - T_2) / (r_{01} + r_{12})$ .  
 $P_{01} = (T_0 - T_1) \kappa_{01} / d_{01}$ . <<conductive>>  
 $r_{01} = d_{01} / \kappa_{01}$ . << $\kappa_{01} = 0. \text{ W/m}^\circ\text{C}$ >>.   
 $P_{12} = (T_1 - T_2) \kappa_{12} S_{12}$ . <<convective>>  
 $r_{12} = 1 / S_{12} \kappa_{12}$ . << $\kappa_{12} (\text{air}) \doteq 7 \text{ W/m}^\circ\text{C}$ >>.   
 $P_{02} = (T_0 - T_2) \kappa_{02} S_{02}$ . <<convective>>  
 $r_{02} = 1 / S_{02} \kappa_{02}$ . << $\kappa_{02} (\text{air}) \doteq 7 \text{ W/m}^\circ\text{C}$ >>.

\* (7)  $t_H \doteq E_H / (Q_s - \langle Q_L(T_0) + Q_L(T_M) \rangle / 2)$ . <<coarse estimation>>.

A coarse heating time could be estimated by heat flow time constant.

heating time constant (example):



$$\tau = r_{OH} C_{OH} = 33946s = 9.4 \text{ hour.}$$

$C_{OH} = 130 \text{ Kg} \times 4.178 \text{ KJ/Kg}^\circ\text{C}$ , <<heat capacity of  $\text{H}_2\text{O}$  of 130Kg>>

heat input  $J$  area  $\equiv S_V = 0.2 \text{ m} \times 4.0 \text{ m}$ .  $J = \kappa_V S_V [T_f - T_m]$ .  $\rightarrow r_{OH} \equiv [T_f - T_m] / J = 1 / \kappa_V S_V$ .

$r_{OH} = 1 / (20 \text{ W/m}^2\text{C} \times 0.2 \text{ m} \times 4.0 \text{ m}) = 0.0625$ . <<convective heat resistor of water>>

[http://www.engineeringtoolbox.com/convective-heat-transfer-d\\_430.html](http://www.engineeringtoolbox.com/convective-heat-transfer-d_430.html)

$T_i = 10^\circ\text{C}$  (initial)  $\rightarrow T_f = 60^\circ\text{C}$  (final)  $T_m = 40^\circ\text{C} \rightarrow \ln(\langle 60-40 \rangle / \langle 60-10 \rangle) = 0.92 \tau$ .

$10^\circ\text{C} \rightarrow 50^\circ\text{C}$	$10^\circ\text{C} \rightarrow 60^\circ\text{C}$	$10^\circ\text{C} \rightarrow 70^\circ\text{C}$	$10^\circ\text{C} \rightarrow 80^\circ\text{C}$	$10^\circ\text{C} \rightarrow 100^\circ\text{C}$
$\ln(1/4) = 1.39$	$\ln(2/5) = 0.92$	$\ln(3/6) = 0.69$	$\ln(4/7) = 0.56$	$\ln(6/9) = 0.41$

Heating time is serious important, which should be improved by design change.

② This article is abridged due to doubtful measurement environments.

Example-5)

inner blackbody box size =  $0.46 \text{ m} \times 0.36 \text{ m} \times 0.18 \text{ m}$ ; opening area  $S_s = 0.46 \times 0.36 = 0.16 \text{ m}^2$ .

input heat amount  $Q_s = 900 \text{ W/m}^2 \times 0.16 \text{ m}^2 = 150 \text{ W}$ .  $\rightarrow 80^\circ\text{C}$  <observing 2011/2/3 in Japan>.

cooling radiation area  $S_L = 2(0.46 \times 0.36) + 2(0.46 \times 0.18) + 2(0.18 \times 0.36) = 0.312 \text{ m}^2$ .

(1) convection heat flow into exterior air  $Q_{LC} = S_L J = 0.312 \text{ m}^2 \times 7 \text{ W/m}^2\text{K}$ . <negligible>

(2) radiation rate of material surface  $@ \doteq 0.5?$ .

Max cooling radiation amount  $Q_s = Q_L = S_L @ \sigma T^4$ .  $\rightarrow T \doteq 87^\circ\text{C}$ , observing =  $80^\circ\text{C}$ .

\*reference site on heat calculation.

<http://www.hakko.co.jp/qa/qakit/html/s01050.htm>

③ [1]: Solar Heater the physics fundamental.

(b) green house method of @ <heat (infrared ray) reflecting wall  $\equiv \text{HW}$ >.

This method seems good at a glance, however there might be a difficulty.

It's a blackbody radiation of semi-transparent HW (heat input window)-itself.

The window become no-green house function at saturated temperature.

☞: This short report is still insufficient to describe systematic design calculator. Please wait for a while.